MONTHLY EM&A REPORT

OSCAR Bioenergy Joint Venture

Contract No. EP/SP/61/10
Organic Resources Recovery
Centre (Phase 1):
Seventy-second Monthly EM&A
Report

1 May 2021 - 31 May 2021

Environmental Resources Management

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Meinhardt Infrastructure and Environment Limited

Organic Resources Recovery Centre, Phase I

Monthly EM&A Report (1 May 2021 – 31 May 2021)

(June 2021)

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Date: 15 June 2021

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Reference 0279222

For and on behalf of ERM-Hong Kong, Limited		
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EXECUTIVE SUMMARY

The construction works of *No. EP/SP/61/10 Organic Resources Recovery Centre Phase 1 (the Project)* commenced on 21 May 2015. This is the 72nd monthly Environmental Monitoring and Audit (EM&A) report presenting the EM&A works carried out during the period from 1 to 31 May 2021 in accordance with the EM&A Manual. Substantial completion of the construction works was confirmed on 3 December 2018. In the meantime, the operation phase EM&A programme had commenced in March 2019. Substantial Completion in respect of substantial part of the Works was confirmed on 24 February 2020. The construction phase EM&A programme was completed in the end of February 2020.

Summary of Works undertaken during the Reporting Month

Works undertaken in the reporting month included:

- Operation of the Project, including organic waste reception, and operation
 of the pre-treatment facilities, anaerobic digesters, composting facilities,
 air pollution control systems, on-line emission monitoring system for the
 Centralised Air Pollution Control Unit (CAPCS), Co-generation Units
 (CHP)s and Ammonia Stripping Plant (ASP), and the wastewater
 treatment plant; and
- Process fine-tune, including adjustment of the ASP with new treatment media, modification of Continuous Environmental Monitoring System (CEMS) and Supervisory Control and Data Acquisition System (SCADA) rectification and improvement works following equipment failures and the alteration of different operation modes and measures to adapt to the high variation of SSOW nature and sources.

Environmental Monitoring and Audit Progress

Air Quality Monitoring

Exceedances on NO_x, SO₂ and VOC from CHP and CO, NO_x, VOC and NH₃ from ASP were recorded on the on-line monitoring system. It should be noted that measurements recorded under abnormal operating conditions, e.g. start up and stopping of stacks, unstable operation, test runs and interference of sensor, are disregarded.

Exceedances in emission parameters of CHP were found to be a result of low biogas loading and unstable performance at CHP. The exceedances of ASP were found to be a result of malfunction of incomplete combustion of biogas at ASP.

The Contractor has implemented mitigation measures to control the exceedance including regular maintenance of the CHP by the supplier and regular fine-tuning, finding better and more feedstock to increase biogas loading and testing at ASP to optimise combustion efficiency and overall performance.

The Contractor is recommended to closely monitor the processes of the modification of the CHP and ASP and the post-modification monitoring of emission level to avoid any exceedance.

Water Quality

No non-compliance to the effluent discharge limit stipulated in the discharge licence issued by the EPD under the *Water Pollution Control Ordinance* was recorded during this reporting period.

Waste Management

Waste generated from the operation of the Project includes chemical waste, waste generated from pre-treatment process and general refuse.

4,000 L of chemical waste was collected by licenced waste collector from the operation of the Project.

671.03 tonnes of waste generated from pre-treatment process from the operation of the Project was disposed of at landfill. Among the recyclable waste generated from pre-treatment process from the operation of the Project, 0.00 tonne of metals, 0.00 tonnes of papers/ cardboard packing and 0.00 tonne of plastics were sent to recyclers for recycling during the reporting period.

Around 2.76 tonnes of general refuse from the operation of the Project was disposed of at landfill. Among the recycled general refuse from the operation of the Project, 0.00 tonne of metals, 0.00 tonne of papers/ cardboard packing and 0.00 tonne of plastics were sent to recyclers for recycling during the reporting period.

Findings of Environmental Site Audit

A summary of the monitoring activities undertaken in this reporting period is listed below:

Joint Environmental Site Inspections

1 time

1 monthly joint environmental site inspections were carried out by the representatives of the Contractor and the MT. The IEC and ER were also present at the joint inspections on 21 May 2021. The environmental control/mitigation measures (related to air quality, water quality, waste (including land contamination prevention), hazard-to-life and landscape and visual) recommended in the approved EIA Report and the EM&A Manual were properly implemented by the Contractor during the reporting month.

Environmental Exceedance/Non-conformance/Compliant/Summons and Prosecution

Exceedances for the air emission limits for the CHP and ASP stacks were recorded during the reporting period.

No complaint/ summon/prosecution was received in this reporting period.

Future Key Issues

Activities to be undertaken in the next reporting month include:

- Operation of the Project.
- Modification of the CHP and ASP to control the air emission.

1 INTRODUCTION

ERM-Hong Kong, Limited (ERM) was appointed by OSCAR Bioenergy Joint Venture (the Contractor) as the Environmental Team (ET) to undertake the construction Environmental Monitoring and Audit (EM&A) programme for the *Contract No. EP/SP/61/10 of Organic Waste Treatment Facilities Phase I,* which the project name has been updated to *Organic Resources Recovery Centre (Phase I) (the Project)* since November 2017. ERM was also appointed by the Contractor to undertake the operation EM&A programme starting 1 March 2019.

1.1 PURPOSE OF THE REPORT

This is the 72nd EM&A report which summarises the monitoring results and audit findings for the EM&A programme during the reporting period from 1 to 31 May 2021.

1.2 STRUCTURE OF THE REPORT

The structure of the report is as follows:

Section 1: Introduction

It details the scope and structure of the report.

Section 2: Project Information

It summarises the background and scope of the Project, site description, project organisation and status of the Environmental Permits (EP)/licences.

Section 3: Environmental Monitoring and Audit Requirements

It summarises the environmental monitoring requirements including monitoring parameters, programmes, methodologies, frequency, locations, Action and Limit Levels, Event/Action Plans, as well as environmental audit requirements as recommended in the EM&A Manual and approved EIA report.

Section 4: Monitoring Results

It summarises monitoring results of the reporting period.

Section 5: Site Audit

It summarises the audit findings of the environmental as well as landscape and visual site audits undertaken within the reporting period.

Section 6: Environmental Non-conformance

It summarises any exceedance of environmental performance standard, environmental complaints and summons received within the reporting period. Section 7: Further Key Issues

It summarises the impact forecast for the next reporting month.

Section 8: Conclusions

2 PROJECT INFORMATION

2.1 BACKGROUND

The Organic Resources Recovery Centre (ORRC) Phase I development (hereinafter referred to as "the Project") is to design, construct and operate a biological treatment facility with a capacity of about 200 tonnes per day and convert source-separated organic waste from commercial and industrial sectors (mostly food waste) into compost and biogas through proven biological treatment technologies. The location of the Project site is shown in *Annex A*.

The environmental acceptability of the construction and operation of the Project had been confirmed by findings of the associated Environmental Impact Assessment (EIA) Study completed in 2009. The Director of Environmental Protection (DEP) approved this EIA Report under the *Environmental Impact Assessment Ordinance* (EIAO) (Cap. 499) in February 2010 (Register No.: AEIAR-149/2010) (hereafter referred to as the approved EIA Report). Subsequent Report on Re-assessment on Environmental Implications and Report on Re-assessment on Hazard to Life Implications were completed in 2013, respectively.

An Environmental Permit (EP) (No. EP-395/2010) was issued by the DEP to the EPD (Project Team), the Permit Holder, on 21 June 2010 and varied on 18 March 2013 (No. EP-395/2010/A) and 21 May 2013 (No. EP-395/2010/B), respectively. The Design Build and Operate Contract for the ORRC Phase 1 (Contract No. EP/SP/61/10 Organic Resources Recovery Centre (Phase 1) (the Contract)) was awarded to SITA Waste Services Limited, ATAL Engineering Limited and Ros-Roca, Sociedad Anonima jointly trading as the OSCAR Bioenergy Joint Venture (OSCAR or the Contractor). A Further EP (No. FEP-01/395/2010/B) was issued by the DEP to the OSCAR on 16 February 2015. Variation to both EPs (Nos. EP-395/2010/B and FEP-01/395/2010/B) were made in December 2015. The latest EPs, Nos. EP-395/2010/C and FEP-01/395/2010/C, were issued by the DEP on 21 December 2015.

Under the requirements of Condition 5 of the EP (No. FEP-01/395/2010/C), an Environmental Monitoring and Audit (EM&A) programme as set out in the approved EM&A Manual (hereinafter referred to as EM&A Manual) is required to be implemented during the construction and operation of the Project. ERM-Hong Kong, Ltd (ERM) has been appointed by OSCAR as the Environmental Team (ET) for the construction phase EM&A programme and the Monitoring Team (MT) for the operation phase EM&A programme for the implementation of the EM&A programme in accordance with the requirements of the EP and the approved EM&A Manual.

The construction works commenced on 21 May 2015. The operation phase of

the EM&A programme commenced on 1 March 2019 (1). The construction phase EM&A programme was completed in the end of February 2020.

2.2 GENERAL SITE DESCRIPTION

The Project Site is located at Siu Ho Wan in North Lantau with an area of about 2 hectares. The layout of the Project Site is illustrated in *Annex A*. The facility received and treated an average of 100 tonnes of source separated organic waste per day during the reporting month.

2.3 MAJOR ACTIVITIES UNDERTAKEN

A summary of the major activities undertaken in the reporting period is shown in *Table 2.1*.

Table 2.1 Summary of Activities Undertaken in the Reporting Period

Activities Undertaken in the Reporting Period

- Systems being operated waste reception, pre-treatment, CAPCS extraction, the digesters, the centrifuge, , the composting tunnels the desulphurisation, the emergency flare, the CHPs, the ASP and the biological waste water treatment plant (about 100-130 t/d SSOW input); and
- Process fine-tune adjustment of the ASP operational parameters with new treatment media, CEMS/SCADA modification and improvement work following equipment failures and the alteration of different operation modes and measures to adapt to the high variation of SSOW nature and sources.

2.4 PROJECT ORGANISATION AND MANAGEMENT STRUCTURE

The project organisation chart and contact details are shown in *Annex B*.

2.5 STATUS OF ENVIRONMENTAL APPROVAL DOCUMENTS

A summary of the valid permits, licences, and/or notifications on environmental protection for this Project is presented in *Table 2.2*.

Table 2.2 Summary of Environmental Licensing, Notification and Permit Status

Permit/ Licences/	Reference	Validity Period	Remarks
Notification			
Environmental	FEP-01/395/2010/C	Throughout the	Permit granted on 21
Permit		Contract	December 2015
Effluent Discharge	WT00024352-2016	3 June 2016 - 30	Approved on 3 June
License		June 2021	2016
Chemical Waste	WPN 5213-961-	Throughout the	Approved on 10
Producer Registration	O2231-02	implementation of	November 2017
		the Project	

As some of the minor items are yet to be closed out in March 2019, the construction phase EM&A programme and Operation Phase EM&A programme were undertaking in parallel in March 2019.

Permit/ Licences/	Reference	Validity Period	Remarks
Notification			
Waste Disposal	Account number:	Throughout the	-
Billing Account	702310	Contract	

3 ENVIRONMENTAL MONITORING AND AUDIT REQUIREMENTS

3.1 ENVIRONMENTAL MONITORING

The air quality (including odour) monitoring to be carried out during the commissioning and operation phase of the Project are described below. Although water quality monitoring is not required for the operation phase under the EM&A programme, there are water quality monitoring requirement under the Water Discharge Licence of the plant under the *Water Pollution Control Ordinance* (WPCO). As part of this EM&A programme, the monitoring results will be reviewed to check the compliance with the WPCO requirements.

3.1.1 Air Quality

According to the EM&A Manual and EP requirements, stack monitoring are required during the commissioning and operation phase of the Project.

On-line monitoring (using continuous environmental monitoring system (CEMS) shall be carried out for the centralised air pollution unit (CAPCS), cogeneration units (CHP) and the ammonia stripping plant (ASP) during the commissioning and operation phase. The calibration certificate for the online monitoring equipment is provided in *Annex C*.

The monitoring data is transmitted instantaneously to EPD (Regional Office) by telemetry system.

When the on-line monitoring for certain parameter cannot be undertaken, monitoring will be carried out using the following methodology approved by the EPD.

Table 3.1 Sampling and Laboratory Analysis Methodology

Parameters	Method	Stacks to be Monitored
Gaseous and vaporous organic	USEPA Method 18	• CAPCS
substances (including methane)		• CHP
		• ASP
Particulate	USEPA Method 5	• CAPCS
		• CHP
		• ASP
Carbon monoxide (CO)	USEPA Method 10	• CHP
		• ASP
Nitrogen oxides (NO _x)	USEPA Method 7E	• CHP
		• ASP
Sulphur dioxide (SO ₂);	USEPA Method 6	• CHP
		• ASP
Hydrogen chloride (HCl)	USEPA Method 26A	• CHP
		• ASP

Parameters	Method	Stacks to be Monitored
Hydrogen fluoride (HF)	USEPA Method 26A	• CHP
		• ASP
Oxygen (O ₂);	USEPA Method 3A	• CAPCS
		• CHP
		• ASP
Velocity and Volumetric Flow	USEPA Method 2	• CAPCS
		• CHP
		• ASP
Ammonia (NH ₃)	USEPA CTM 027	• ASP
Odour (including NH ₃ and H ₂ S)	EN 13725	• CAPCS
Water vapour content (continuous	USEPA Method 4	• CAPCS
measurement of the water vapour		• CHP
content should not be required if the sample exhaust gas is dried before the emissions are analysed)		• ASP
Temperature	USEPA Method 4	• CAPCS
		• CHP
		• ASP

With reference to the EM&A Manual, the air emission of the stacks shall meet the following emission limits as presented in *Tables 3.2* to *3.5*.

Table 3.2 Emission Limit for CAPCS Stack

Parameter	Emission Level (mg/Nm³) (a)
VOCs (including methane)	680
Dust (or Total Suspended Particulates (TSP))	6
Odour (including NH ₃ & H ₂ S)	220 (b)
Notes:	
(a) Hourly average concentration	
(b) The odour unit is OU/Nm ³	

Table 3.3 Emission Limit for CHP Stack

Parameter	Maximum Emission Level (mg/Nm³) (a) (b)	
Dust (or Total Suspended Particulates)	15	
Carbon Monoxide	650	
NO_x	300	
SO ₂	50	
NMVOCs (c)	150	
VOCs (including methane) (d)	1,500	
HCl	10	
HF	1	

Notes:

- (a) All values refer to an oxygen content in the exhaust gas of 6% and dry basis.
- (b) Hourly average concentration
- (c) NMVOCs should be monitored by gas sampling and laboratory analysis at an agreed interval. For the first 12 months (starting from August 2019), monitoring should be carried out at quarterly intervals. The monitoring frequency should then be reduced to half-yearly for next 12 months (starting from August 2020).

Para	ameter	Maximum Emission Level (mg/Nm³) (a) (b)
(d)	The VOCs emission limit include methane	e as biogas is adopted as fuel in the combustion

Table 3.4 Emission Limit for ASP Stack

Maximum Emission Level (mg/Nm³) (a) (b) 5 100
100
200
200
50
20
35
10
1

Notes:

- (a) All values refer to an oxygen content in the exhaust gas of 11% and dry basis.
- (b) Hourly average concentration
- (c) The VOCs emission limit include methane as biogas is adopted as fuel in the combustion process.

Table 3.5 Emission Limit for Standby Flaring Gas Unit (1)

Parameter	Maximum Emission level (mg/Nm³) (a) (b)
Dust (or Total Suspended Particulates)	5
Carbon Monoxide	100
NO_x	200
SO_2	50
VOCs (including methane) (c)	20
HCl	10
HF	1

Notes:

- (a) All values refer to an oxygen content in the exhaust gas of 11% and dry basis.
- (b) Hourly average concentration
- (c) The VOCs emission limit include methane as biogas is adopted as fuel in the combustion process.

3.1.2 *Odour*

To determine the effectiveness of the proposed odour mitigation measures and to ensure that the operation of the ORRC1 will not cause adverse odour impacts, odour monitoring of the CAPCS stack (see *Section 3.1.1*) and odour patrol will be carried out.

Odour patrol shall be conducted by independent trained personnel/ competent persons in summer months (i.e. from July to September) for the first two operational years of ORRC1 at monthly intervals along an odour

A standby facility. Only operate when the CHPs are not in operation or when the biogas generated exceeded the utilisation rate of the CHPs.

patrol route at the Project Site boundary as shown in $Annex A^{(1)}$.

The perceived odour intensity is divided into 5 levels. *Table 3.6* describes the odour intensity for different levels.

Table 3.6 Odour Intensity Level

Level	Odour Intensity
0	Not detected. No odour perceived or an odour so weak that it cannot be easily characterised or described
1	Slight identifiable odour, and slight chance to have odour nuisance
2	Moderate identifiable odour, and moderate chance to have odour nuisance
3	Strong identifiable, likely to have odour nuisance
4	Extreme severe odour, and unacceptable odour level

Table 3.7 shows the action level and limit level to be used for odour patrol. Should any exceedance of the action and limit levels occurs, actions in accordance with the event and action plan in *Table 3.8* should be carried out.

Table 3.7 Action and Limit Levels for Odour Nuisance

Parameter	Action Level	Limit Level
Odour Nuisance (from odour patrol)	When one documented compliant is received ^(a) , or Odour Intensity of 2 is measured from odour patrol.	Two or more documented complaints are received ^(a) within a week; or Odour intensity of 3 or above is measured from odour patrol.

Note:

(a) Once the complaint is received by the Project Proponent (EPD), the Project Proponent would investigate and verify the complaint whether it is related to the potential odour emission from the ORRC1 and its on-site wastewater treatment unit.

Table 3.8 Event and Action Plan for Odour Monitoring

Event	Action		
	Person-in-charge of Odour Monitoring	Project Proponent (a)	
Action Level			
Exceedance of action level (Odour Patrol)	 Identify source/reason of exceedance; Repeat odour patrol to confirm finding. 	 Carry out investigation to identify the source/reason of exceedance. Investigation should be completed within 2 weeks; Rectify any unacceptable practice; Implement more mitigation measures if necessary; Inform Drainage Services Department (DSD) or the operator of the Siu Ho Wan Sewage Treatment Works (SHWSTW) if exceedance is considered to be caused by 	

⁽¹⁾ The odour patrol route was changed during this reporting period to include sampling points that are frequently visited by visitors and eliminate sampling points that are not visited by visitors.

Event	Action			
	Person-in-charge of Odour Monitoring	Project Proponent (a)		
	-	the operation of the SHWSTW.		
		5. Inform North Lantau Refuse Transfer Station (NLTS) operator if exceedance is considered to be caused by the operation of NLTS.		
Exceedance of action level (Odour Complaints)	 Identify source/reason of exceedance; Carry out odour patrol to determinate odour intensity. 	1. Carry out investigation and verify the complaint whether it is related to potential odour emission from the nearby SHWSTW;		
		2. Carry out investigation to identify the source/reason of exceedance. Investigation should be completed within 2 weeks;		
		3. Rectify any unacceptable practice;		
		4. Implement more mitigation measures if necessary;		
		5. Inform DSD or the operator of the SHWSTW if exceedance is considered to be caused by the operation of the SHWSTW.		
		6. Inform NLTS operator if exceedance is considered to be caused by the operation of NLTS.		
Limit Level				
Exceedance of limit level	 Identify source/reason of exceedance; Inform EPD; 	Carry out investigation to identify the source/reason of exceedance. Investigation should be completed within 2 week;		
	Repeat odour patrol to confirm findings;	2. Rectify any unacceptable practice;		
	4. Increase odour patrol	3. Formulate remedial actions;		
	frequency to bi-weekly;	4. Ensure remedial actions properly		
	5. Assess effectiveness of remedial action and keep EPD informed of the results;6. If exceedance stops, cease additional odour patrol.	implemented;5. If exceedance continues, consider what more/enhanced mitigation measures should be implemented;6. Inform DSD or the operator of the		
Note:	additional odour pation.	SHWSTW if exceedance is considered to be caused by the operation of the SHWSTW.		

Note:

(a) Project Proponent shall identify an implementation agent.

3.2 SITE AUDIT

Environmental mitigation measures (related to air quality, water quality, waste, land contamination, hazard-to-life, and landscape and visual) to be implemented during the operation phase of the Project are recommended in the approved EIA Report and EM&A Manual and are summarised in *Annex D*. Monthly site audits for operation phase will be carried out to check the implementation of these measures.

3.2.1 Water Quality

Compliance audits are to be undertaken to ensure that a valid discharge licence has been issued by EPD prior to the discharge of effluent from the operation of the Project site. The audit shall be conducted to ensure that the effluent quality is in compliance with the discharge licence requirements. The effluent quality shall meet the discharge limits as described in *Table 3.9*.

Table 3.9 Discharge Limits for Effluent

Parameters	Discharge Limit (mg/L)
Flow Rate (m ³ /day)	685
pH (pH units)	6-10 (a)
Suspended Solids	800
Biochemical Oxygen Demand (5 days, 20°)	800
Chemical Oxygen Demand	2,000
Oil & Grease	40
Total Nitrogen	200
Total Phosphorus	50
Surfactants (total)	25
Note:	
(a) Range.	

3.2.2 Landscape and Visual

In accordance with EM&A Manual, the landscape and visual mitigation measures shall be implemented.

For operation phase, site inspection shall be conducted once a month for the first year of operation of the Project. All measures as stated in the implementation schedule of the EM&A Manual (see *Annex D*), including compensatory planting, undertaken by both the Contractor and the specialist Landscape Sub-Contractor during the first year of the operation phase shall be audited by a Registered Landscape Architect (RLA) to ensure compliance with the intended aims of the measures and the effectiveness of the mitigation measures. After the one-year maintenance period, the landscape maintenance and monitoring shall be carried out by the Contractor.

4 MONITORING RESULTS

4.1 AIR QUALITY

4.1.1 Commissioning Phase Monitoring

Monitoring results of air quality parameters from stack emissions of the centralised air pollution control system, the ammonia stripping plant and the cogeneration units will be provided once available to show compliance with the monitoring requirements stated in the EM&A Manual (Rev. F) to support the termination of the commissioning phase EM&A programme.

4.1.2 Operation Phase Monitoring

The concentrations of concerned air pollutants emitted from the stacks of the CAPCS, CHP, and ASP during the reporting period are monitored on-line by the continuous environmental monitoring system (CEMS). During the reporting period, there is no need to operate the standby flare and therefore no monitoring of the flare stack was undertaken.

With reference to the emission limits shown in *Tables 3.2, 3.3* and *3.4*, the hourly average concentrations and the number of exceedances of the concerned air emissions monitored for the CAPCS, CHP and ASP during this reporting period are presented in *Tables 4.1* to *4.5*.

It should be noted that measurements recorded under abnormal operating conditions, e.g. start up and stopping of stacks, unstable operation, test runs and interference of sensor, are disregarded.

Table 4.1 Hourly Average of Parameters Recorded for CAPCS

Parameter	Range of Hourly Average Conc. (mg/Nm³)	Emission Limit (mg/Nm³)	Exceedance Identified	Remarks
VOCs (including methane)	11.21 - 16.98	680	Nil	Nil
Dust (or TSP)	0.00 - 0.43	6	Nil	Nil
Odour (including NH ₃ & H ₂ S) (a)	0.00 - 180.06	220	Nil	Nil
Note:				
(a) The odour unit is OU/Nm^3 .				

Table 4.2 Hourly Average of Parameters Recorded for CHP 1

Parameter	Range of Hourly Average Conc. (mg/Nm³) (a)	Max. Emission Limit (mg/Nm³)	Exceedance Identified	Remarks
Dust (or TSP)	0 - 1	15	Nil	Nil
Carbon Monoxide	0 - 431	650	Nil	Nil
NO _x	0 - 354	300	Identified (d)	System unstable (e.g. low efficiency, unstable column temperature)
SO ₂	0 - 145	50	Identified (e)	Desulpurisation system tripped and resumed to normal after urgent maintenance.
NMVOCs (b)	Nil	150	-	Nil
VOCs (including methane) (c)	0 - 890	1,500	Nil	Nil
HCl	0 - 0	10	Nil	Nil
HF	0 - 1	1	Nil	Nil

Notes:

- (a) All values refer to an oxygen content in the exhaust gas of 6% and dry basis.
- (b) No sampling was undertaken at CHP 1 as biogas production rate could not sustain the operation of the CHP stack for the scheduled sampling on 8 February 2021.
- (c) The VOCs emission limit include methane as biogas is adopted as fuel in the combustion process.
- (d) Dates with exceedances on NO_x (number of exceedances on the day) were identified on 6 (2), 11 (2), 12 (11), 13 (7) and 18 (2) May 2021.
- (e) Dates with exceedances on SO_2 (number of exceedances on the day) were identified on 21 (7) and 26 (4) May 2021.

Table 4.3 Hourly Average of Parameters Recorded for CHP 2

Parameter	Range of Hourly Average Conc. (mg/Nm³)		Exceedance Identified	Remarks
Dust (or TSP)	0 - 4	15	Nil	Nil
Carbon Monoxide	0 - 288	650	Nil	Nil
NO_x	0 - 298	300	Nil	Nil
SO ₂	0 - 51	50	Identified (d)	Desulpurisation system tripped and resumed to normal after urgent maintenance.
NMVOCs (b)	6.0	150	Nil	Nil
VOCs (including methane) (c)	0 - 1,441	1,500	Nil	Nil
HCl	0 - 2	10	Nil	Nil
HF	0 - 1	1	Nil	Nil

Notes:

- (a) All values refer to an oxygen content in the exhaust gas of 6% and dry basis.
- (b) Bi-annual sampling of NMVOCs was conducted in CHP 2 on 8 February 2021. No

Parameter	Range of	Max.	Exceedance	Remarks
	Hourly Average	Emission	Identified	
	Conc. (mg/Nm ³)	Limit		
	(a) (b)	(mg/Nm^3)		

exceedance was identified.

Table 4.4 Hourly Average of Parameters Recorded for CHP 3

Parameter	Range of Hourly Average Conc. (mg/Nm³) (a)	Max. Emission Limit (mg/Nm³)	Exceedances Identified	Remarks
Dust (or TSP)	0 - 4	15	Nil	Nil
Carbon Monoxide	0 - 225	650	Nil	Nil
NO _x	0 - 438	300	Identified (d)	System unstable (e.g. low efficiency, unstable column temperature)
SO ₂	0 - 139	50	Identified (e)	Desulpurisation system tripped and resumed to normal after urgent maintenance.
NMVOCs (b)	Nil	150	Nil	Nil
VOCs (including methane) (c)	0 – 1,591	1,500	Identified (f)	System unstable (e.g. low efficiency, unstable column temperature)
HCl	0 - 3	10	Nil	Nil
HF	0 - 1	1	Nil	Nil

Notes:

- (a) All values refer to an oxygen content in the exhaust gas of 6% and dry basis.
- (b) No sampling was undertaken at CHP 3 as biogas production rate could not sustain the operation of the CHP stack for the scheduled sampling on 8 February 2021.
- (c) The VOCs emission limit include methane as biogas is adopted as fuel in the combustion process.
- (d) Dates with exceedances on NO_x (number of exceedances on the day) were identified on 1 (17), 2 (17), 3 (3), 4 (10), 5 (13), 6 (3), 17 (3), 18 (7), 20 (1), 21 (10), 22 (15), 23 (17), 24 (12), 25 (7) and 26 (8) May 2021.
- (e) Dates with exceedances on SO₂ (number of exceedances on the day) were identified on 21 (7) and 26 (4) May 2021.
- (f) Dates with exceedances on VOC (number of exceedances on the day) were identified on 18 (1), 22 (1) and 26 (1) May 2021.

⁽c) The VOCs emission limit include methane as biogas is adopted as fuel in the combustion process.

⁽d) Date with exceedances on SO₂ (number of exceedances on the day) was identified on 7 (1) May 2021.

Table 4.5 Hourly Average of Parameters Recorded for ASP

Parameter	Range of Hourly Average Conc. (mg/Nm³) (a)	Max. Emission Limit (mg/Nm³)	Exceedances Identified	Remarks
Dust (or TSP)	0.0 - 0.0	5	Nil	Nil
Carbon Monoxide	0 - 1,278	100	Identified (c)	System instability due to unstable column temperature.
NO _x	0 - 233	200	Identified (d)	System instability due to unstable column temperature.
SO ₂	0 - 47	50	Nil	Nil
VOCs (including methane) (b)	0 - 118	20	Identified (e)	System instability due to unstable column temperature.
NH ₃	0 - 234	35	Identified (f)	System instability due to unstable column temperature.
HCl	0 - 0	10	Nil	Nil
HF	0 - 1	1	Nil	Nil

Notes:

- (a) All values refer to an oxygen content in the exhaust gas of 11% and dry basis.
- (b) The VOCs emission limit include methane as biogas is adopted as fuel in the combustion process.
- (c) Date with exceedances on CO (number of exceedances on the day) was identified on 7 (2) May 2021.
- (d) Dates with exceedances on NO_x (number of exceedances on the day) were identified on 5 (1) May 2021.
- (e) Dates with exceedances on VOC (number of exceedances on the day) was identified on 7(2) May 2021.
- (f) Date with exceedances on NH₃ (number of exceedances on the day) were identified on 1 (2), 2 (3), 4 (13), 5 (7), 6 (1), 7 (4), 8 (4), 9 (6), 11 (1), 15 (1), 20 (5), 21 (12), 23 (1) and 26 (2) May 2021.

4.2 ODOUR

4.2.1 Operation Phase Monitoring

No odour patrol was required to be conducted for this reporting period.

4.3 WATER QUALITY

4.3.1 Operation Phase Monitoring

Effluent discharge was sampled monthly from the Effluent Storage Tank as stipulated in the operation phase discharge licence. The results of the discharge sample is recorded in *Table 4.6*.

Table 4.6 Results of the Discharge Sample

Parameters	Discharged Effluent Concentration (mg/L)	O	Compliance with Discharge Limit
pH (pH units)	7.61 - 8.23	6-10 (a)	Yes
Suspended Solids (b)	183	800	Yes
Biochemical Oxygen Demand (5 days, 20°) ^(b)	17	800	Yes
Chemical Oxygen Demand (b)	1,070	2,000	Yes
Oil & Grease (b)	<5	40	Yes
Total Nitrogen (b)	84.0	200	Yes
Total Phosphorus (b)	37.5	50	Yes
Surfactants (total) (b)	<1.0	25	Yes

Notes:

- (a) Daily Average.
- (b) Effluent sample was collected on 13 May 2021.

No exceedance of discharge limit was recorded during the reporting period.

4.4 WASTE MANAGEMENT

4.4.1 Operation Phase Monitoring

Wastes generated from the operation of the Project include chemical waste, wastes generated from pre-treatment process and general refuse (1). Reference has been made to the Monthly Summary Waste Flow Table prepared by the Contractor (see *Annex E*). With reference to the relevant handling records and trip tickets of this Project, the quantities of different types of waste generated from the operation of the Project in the reporting month are summarised in *Table 4.7*.

Table 4.7 Quantities of Waste Generated from the Operation of the Project

Month/Year	Chemical Waste	Waste Gene Pre-treatme		General Refuse		
	Disposal of at CWTC	Disposed of at Landfill (a)	Recycled (b)	Disposed of at Landfill (a)	Recycled (c)	
May 2021	4,000 L	671.03 tonnes	0.00 tonnes	2.76 tonnes (d)	0.00 tonne	

Notes:

- (a) Waste generated from pre-treatment process and general refuse other than chemical waste and recyclables were disposed of at NENT Landfill by sub-contractors.
- (b) Among waste generated from pre-treatment process, 0.00 tonne of metals, 0.00 tonne of papers/ cardboard packing and 0.00 tonne of plastics were sent to recyclers for recycling during the reporting period.
- (c) Among general refuse, 0.00 kg of metals, 0.00 kg of papers/ cardboard packing and 0.00 kg of plastics were sent to recyclers for recycling during the reporting period.
- (d) It was assumed that four 240-litre bins filled with 80% of general refuse were collected at each collection. The general refuse density was assumed to be around $0.15 \, \text{kg/L}$.

Public fill and construction waste may only be generated during maintenance works when there are civil or structural works.

5 SITE AUDIT

5.1 ENVIRONMENTAL SITE AUDIT

5.1.1 *Operation Phase*

The monthly inspection for the operation phase of the Project on 21 May 2021 covered the operation phase environmental site audit. Joint site inspections was conducted by representatives of the Contractor, IEC, and the MT on 21 May 2021 as required for the operation of the Project.

The audits checked the implementation of the recommended mitigation measures for air quality, landscape and visual, water quality, waste (land contamination) and hazard-to-life stated in the Implementation Schedule (see *Annex D*).

Follow-up actions resulting from the last site inspections were generally taken as reported by the Contractor.

Key observations during the reporting period are summarised as follows:

21 May 2021

• No particular observation during this inspection.

Other than the above observations, the Contractor has implemented environmental mitigation measures recommended in the approved EIA Report and EM&A Manual.

5.2 LANDSCAPE AND VISUAL AUDIT

The monthly inspection for the operation phase of the Project on 21 May 2021 also covered the monitoring of landscape and visual mitigation measures, for the operation phase of the Project.

It was confirmed that the necessary landscape and visual mitigation measures during the operation phase as summarised in *Annex D* were generally implemented by the Contractor. No specific observation was found during site inspections on 21 May 2021. No non-compliance in relation to the landscape and visual mitigation measures was identified during the site audits in this reporting period and therefore no further actions are required. The ET/MT will keep track of the EM&A programme to check compliance with environmental requirements and the proper implementation of all necessary mitigation measures.

6.1

SUMMARY OF ENVIRONMENTAL NON-COMPLIANCE AND DEFICIENCIES

Non-compliance of emission limits for CHP and ASP were recorded during the reporting period.

The Contractor has reviewed the organic waste treatment processes (i.e. waste reception, waste pre-treatment, anaerobic digesters, and composting processes) and found that they were operated normally during the reporting period. The Contractor has investigated the air pollution control system and the combustion system of the CHP and ASP and identified the following potential causes for the exceedance.

- (a) The exceedances from CHP 1 occurred mainly when the feedstock quantity was at 40-60% of the optimal treatment quantity, which could hinder the performance of the CHP to achieve optimal efficiency. Therefore, it could not effectively remove NO_x at a certain period of time which leads to the exceedance of NO_x limit at the CHP;
- (b) The exceedances of NO_x and VOC limits at CHP 3 occurred due to equipment tripping and its unstable performance;
- (c) The exceedances of SO₂ limit at the CHPs occurred due to equipment tripping of the desulphurisation system;
- (d) The ASP was experiencing unstable column temperature due to equipment tripping resulting in the incomplete combustion of biogas and NH₃. These have led to the exceedances of CO, NO_x, VOC and NH₃ in ASP.

For item (a), insufficient biogas available for CHP 1 has been identified as a key reason that led to the reduced performance of the CHP, resulting in emission exceedances from the CHP. In this reporting period, the plant has received on average around 120 tonnes of SSOW daily, which is slightly more than received in the last reporting period. Yet, as advised by the Contractor, it is more desirable that the plant can receive at least 150 tonnes of SSOW daily in order to generate sufficient biogas for the CHP to be able to operate at optimal efficiency. The Contractor will continue to liaise with EPD (Food Waste Recycling Group) in their monthly meeting with an aim to explore the possibility of increasing the quantity of SSOW that can be treated daily.

For item (b), unstable performance of the CHP 3 has led to exceedances of NO_x and VOC. Although the Contractor was advised to halt the use of CHP 3 in this reporting period due to its unstable performance, it was used when CHP 2 was under urgent maintenance for about 10 days as sufficient biogas consumption requires the operation of 2 CHPs. The Contractor will continue to avoid the use of CHP 3 and engage with the supplier to carry out on-site inspection of the CHP.

For item (c), The SO₂ exceedances recorded in CHPs were due to tripping of the desulphurisation system, which were stopped temporary for urgent maintenance. The desulphurisation system resumed to normal operation on the day after urgent maintenance.

For item (d), the exceedances of CO, NO_x, VOC and NH₃ were found to be due to unstable column temperature in biogas combustion, which have led to incomplete combustion of biogas and NH3 and hence exceedances in ASP. The Contractor has established a daily communication channel with the overseas ASP supplier, to overcome the fact that the supplier cannot travel to Hong Kong due to travel restriction at the moment. Since January 2021, the Contractor has engaged with the overseas ASP supplier to undertake remote fine-tuning during normal operation of the ASP on a daily basis, focusing on key parameters including wastewater flow rate, NH3 concentration of wastewater, exhaust air flow rate and combustion temperature of the thermal oxidizer. The objective is to determine the desirable operating conditions of the ASP taking into account of the aforementioned key parameters and to devise a standard operating procedure for ASP. In addition, the Contractor continues to carry out maintenance measures as per the supplier's manual. The Contractor will continue to work with the overseas ASP supplier to investigate the reasons for the occasional equipment tripping that has led to unstable column temperature of the thermal oxidizer and, subject to their investigations, replacement of some ASP equipment and/or increased maintenance frequency may be proposed.

The investigation report is presented in *Annex G*.

6.2 SUMMARY OF ENVIRONMENTAL COMPLAINT

No complaint was received during the reporting period.

6.3 SUMMARY OF ENVIRONMENTAL SUMMON AND SUCCESSFUL PROSECUTION

No summon/prosecution was received during the reporting period. The cumulative summons/prosecution log is shown in *Annex F*.

7 FUTURE KEY ISSUES

7.1 KEY ISSUES FOR THE COMING MONTH

Activities to be undertaken for the coming reporting period are:

- Operation of the Project.
- Modification of the CHP and ASP to control the air emission.

8 CONCLUSIONS

This EM&A Report presents the EM&A programme undertaken during the reporting period from **1** to **31 May 2021** in accordance with EM&A Manual (Version F) and requirements of EP (FEP-01/395/2010/C).

For the operation phase, exceedances of the emission limits for CHP and ASP stack monitoring were recorded under normal operating conditions during the reporting period (see *Table 8.1*).

Table 8.1 Exceedances for Stack Emissions

Stack	tack Exceedances During the Reporting Period			
Cogeneration Unit (CHP)	 Exceeded emission limit of NO_x on 1 - 6, 11, 12, 13, 17, 18, 20, 21, 22 23, 24, 25 and 26 May 2021. 			
	• Exceeded emission limit of SO ₂ on 7, 21 and 26 May 2021.			
	• Exceeded emission limit of VOC on 18, 22 and 26 May 2021.			
Ammonia Stripping Plant (ASP)	 Exceeded emission limit of CO on 7 May 2021. 			
	 Exceeded emission limit of NO_x on 5 May 2021. 			
	 Exceeded emission limit of VOC on 7 May 2021. 			
	 Exceeded emission limit of NH₃ on 1, 2, 4, 5, 6, 7, 8, 9, 11, 15, 20, 21, 23 and 26 May 2021. 			

Exceedances in emission parameters of CHP were found to be a result of the occasional low biogas loading at the CHPs and unstable performance of CHP 3. The exceedances of ASP were found to be result of incomplete combustion of biogas at ASP.

The Contractor has implemented mitigation measures to control the exceedance including the continuous monitoring of CHP and ASP to optimise overall performance.

No non-compliance to the effluent discharge limit was recorded during this reporting period.

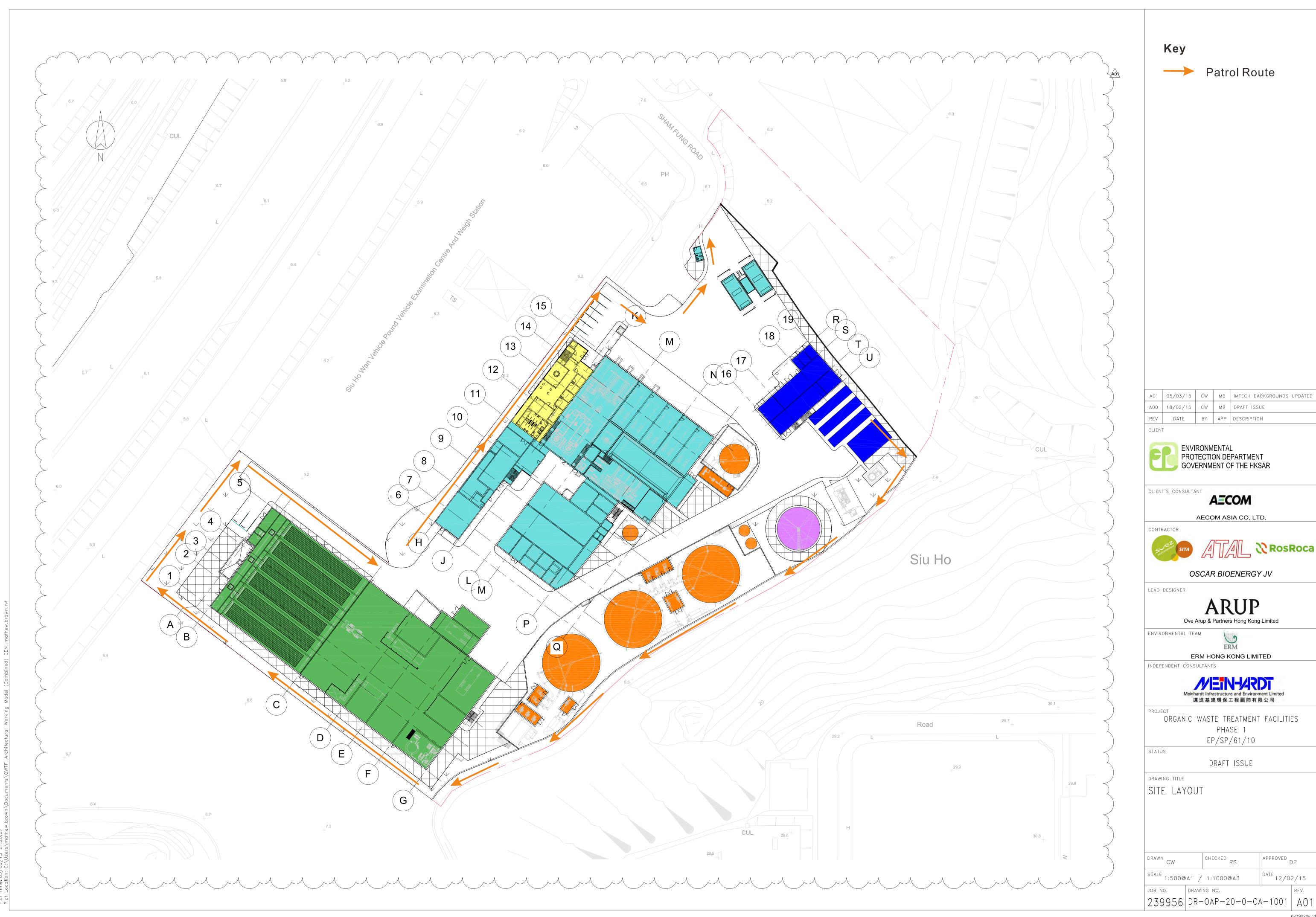
The environmental control / mitigation measures related to air quality, water quality, waste (including land contamination prevention), hazard-to-life and landscape and visual recommended in the approved EIA Report and the EM&A Manual were properly implemented by the Contractor during the reporting month.

Monthly landscape and visual monitoring were conducted in the reporting period. The necessary landscape and visual mitigation measures recommended in the approved EIA Report were generally implemented by the Contractor.

No complaint/summon/prosecution was received.

Annex A

Project Layout

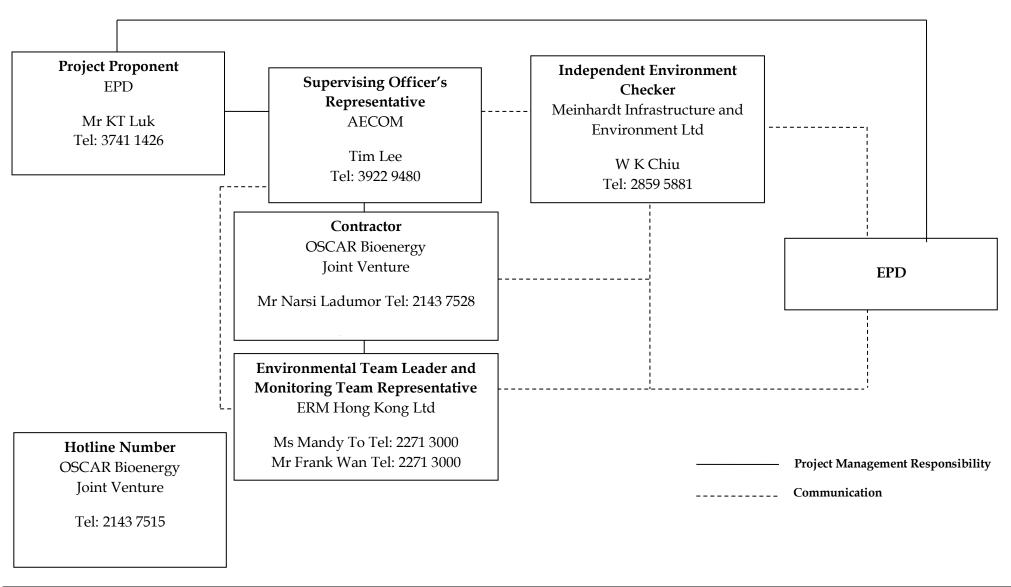


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Annex B

Project Organisation Chart with Contact Details

Project Organization (with contact details)



Annex C

Calibration Certification for the On-line Stack Monitoring System

Annex C1

Calibration Certification for the CEMS

Commissioning Check List 试运行检查项目表 MCS100FT

Cus	stomer data 客户资料				_			
Customer: OSCOR			Plant: OWTF					
Location: SHW								
	Device data 设备资料 Device type 设备类型: Moslo Serial no. 序列号: 1607 Sample probe type 取样探头类型: SFU	1						
2.	Plant data 电厂资料							
Section 标签编号 Orientation of the stack 取样点 方向 Orientation of sample gas probe 取样探头方向		Outside 室外 口 Horizontal 水平口 Horizontal		er cover 保护罩 □ Vertical 垂直 ☑ Vertical 垂直 □		nside 室内 ☑		
	Pressure 压力 _ Plant operating status 电厂运行情况 _	1010_hpa Иогма [G	Sas tempera	ature	烟气温度	E 410 °	С
3.	Prerequisite 系统运行条件		Y	N Ren	narks	备注		
3.1.	Documentation + Delivery co 文件+货物是否齐全	mplete	Ø					
3.2.	Platform at measurement spesuitable dimension? 测量点平台的尺寸是否合适?	ot has	d					
3.3.	If this measurement location legal regulation, has it been acknowledged by an official b如果安装位置需要符合法律法位置是否被官方认可?	oody?	Ø					
3.4.	Customer specific data for parameterization available? 用户对系统参数的特殊要求是	否可行?	d					
3.5.	Cables, tubes and sample lin but not connected? 电缆、管线和取样管线安装但							
3.6.	Compressed air station instal compressed air available? 压缩空气站已安装并且压缩空用?							

4. 1	Preliminary work 预备工作				7
		Y	N	Remarks 备注	
4.1.	Mounting of flanges like described in the Operating Instruction? 法兰安装是否按照图纸?	Ø			
4.2.	Check for damage 检查外部损伤	Ø			
4.3.	Check ambient conditions 检查环境条件	Ø			
4.4.	Check mounting conditions 检查安装条件	D			
4.5.	Check cables / wires for correct installation 检查电缆/电线及其连接状况	D/			
4.6.	Check main power supply voltage 检查总供电电压	Ø	П		
5. F	Periphery 外部设备				
		Y	N	Remarks 备注	
5.1.	Check compressed air supply 检查压缩空气供应	D/			
	Inlet 入口(5 bar):				
6. 5	Sample probe 取样探头	30	70.0	COLUMN TO STATE OF THE STATE OF	
		Υ	N	Remarks 备注	
6.1.	管线和电缆的连接	Ø			
6.2.	Install probe 探头安装	Ø			

7	MCS100FT	-		
	MICC TOUT T	Y	N	Remarks 备注
	Switch on analyzer and wait for warm up 打开分析仪并等待预热	Ø		
7.2.	Check sample conditions 检查样气情况	M		
	Flow rate 流量: 230 l/h			
7.3.	Check zero conditions 检查零点情况	Ø		
	Flow rate 流量: 160 l/h			
7.4.	Perform zero point setting 零点设置	Ø	07	Test results within specification,
7.5.	Perform span test 量程测试	Ø		
7.6.	Parameterize the I/O Module 设置 I/O 模块参数	Ø		
7.7.	Measured values are plausible 测量值是否合理	Ø		
7.8.	Save device data 储存设备数据	Q		
7.9.	Complete Commissioning Sign-Off Sheet 完成试运行签署表	Ø		
7.10	Instruct the operator personnel 操作员培训 Hand over the maintenance manual and check lists 移交维护手册和检查表 - Measurement reading 读取测量值 - Perform customer maintenance 演示维护方法 - Read messages 读取信息	Þ		

8. Measured value

Index	Source	Unit	Range	e 范围	Reading	Output
编号	信号源	单位	Start 开始	End 结束	(actual) 实际读数	value 产值
1	HCL	mg/Nm3	0	(20	60.22 PPM	60,22 ppm
2	HF	ma/Nm3	0	5	4,34 pm	4,34 ppm
3	CO	ma/Nm3	0	1000	128.21ppm	128,20 ppm
4	NO	ma/Nm3	0	500	122.01PPM	122,00 PPh
5	NO ₂	ma/Nm3	0	200	98.81 ppm	98.80 PP4
6	NO _X	ma/Nm3	0	500	4/21/10/13	4/2.12 ma
7	SO ₂	max/Nm3	0	300	83,21 Ppm	83.21 PPH
8	CO ₂	Vol 0/0	0	25	20,010/0	20.01.010
9	H₂O	Vololo	0	40	32.020/0	32,010/0
10	O ₂	10000	0	21	20,950/5	20,950/5
11	TOC	mos/Nm3	0	300	122,01 ppm	122,01 pps
12	NH ₃	ma/Nm3	0	100	53,30 ppm	53,3/pph
13	CH4	ma/Nm3	0	100	112.01 ppm	112.01 PPW
14		1 100		T. Ne	11-10-1-1-1	112011770
15						

temarks 备注		
Date / 1	Name 签名	
Date 日期: 25/7/20/8 Engineer 工程师: Whith	Plant personnel 用户代表:	

(2)

Commissioning Check List 试运行检查项目表 MCS100FT

Cus	stomer data 客户资料					
Customer: Oscar			Plant: OWTF			
	Location: SHW					
	Device data 设备资料 Device type 设备类型: MCS (00FT () Serial no. 序列号: 1607 0494 Sample probe type 取样探头类型: SFU					
2.	Plant data 电厂资料					
Loca	outside ation 标签编号 室外		nder cover Inside 有保护單			
Orie 方向	entation of the stack 取样点 N	al	Vertical 垂直 ☑			
	Horizont 採头方向 水平	al	Vertical 垂直 □			
	Pressure 压力 <u>fo fo</u> Plant operating status 电厂运行情况 <u>Norma</u>	hpa	Gas temperature 烟气温度 <u>410</u> °C			
3.	Prerequisite 系统运行条件	Y	N Remarks 备注			
3.1.	Documentation + Delivery complete 文件+货物是否齐全	Ø				
3.2.	Platform at measurement spot has suitable dimension? 测量点平台的尺寸是否合适?	Ø				
3.3.	If this measurement location is under legal regulation, has it been acknowledged by an official body? 如果安装位置需要符合法律法规,此多位置是否被官方认可?	M				
3.4.	Customer specific data for parameterization available? 用户对系统参数的特殊要求是否可行?	Ø				
3,5.	Cables, tubes and sample line installed but not connected? 电缆、管线和取样管线安装但没有连接	M				
3.6.	Compressed air station installed and compressed air available? 压缩空气站已安装并且压缩空气可以使用?	ŧ 🗹				

4 1	Preliminary work 预备工作				_
7	Telliminary Work Don't Live	Y	N	Remarks 备注	
4.1.	Mounting of flanges like described in the Operating Instruction? 法兰安装是否按照图纸?	Ø			
4.2.	Check for damage 检查外部损伤	Ø			
4.3.	Check ambient conditions 检查环境条件	Ø			
4.4.	Check mounting conditions 检查安装条件	Ø.			
4.5.	Check cables / wires for correct installation 检查电缆/电线及其连接状况	Ø			
4.6.	Check main power supply voltage 检查总供电电压	M			
5. F	Periphery 外部设备				
		Y	N	Remarks 备注	
5.1.	Check compressed air supply 检查压缩空气供应	D			
	Inlet 入口(5 bar): 6 Bar				
6. 5	Sample probe 取样探头				
		Y	N	Remarks 备注	
6.1.	Connect bundle of tubes and cables 管线和电缆的连接	Ø			
6.2.	Install probe 探头安装	A			

7.	MCS100FT	Υ	N	Remarks 备注
7.1.	Switch on analyzer and wait for warm up 打开分析仪并等待预热	<u></u>		Nemans 甘仁
7.2.	Check sample conditions 检查样气情况	d		
	Flow rate 流量: 240 l/h			
7.3.	Check zero conditions 检查零点情况	M		
	Flow rate 流量: 150 l/h	1		
7.4.	Perform zero point setting 零点设置	V		
7.5.	Perform span test 量程测试	Ø		Test results within specification
7.6.	Parameterize the I/O Module 设置 I/O 模块参数	M		1
7.7.	Measured values are plausible 测量值是否合理	Ø		
7.8.	Save device data 储存设备数据	d		
7.9.	Complete Commissioning Sign-Off Sheet 完成试运行签署表	$ \sqrt{} $		
7.10	Instruct the operator personnel 操作员培训 Hand over the maintenance manual and check lists 移交维护手册和检查表 - Measurement reading 读取测量值 - Perform customer maintenance 演示维护方法 - Read messages 读取信息			

8. Measured value

Index	Source	Unit	Range	e 范围	Reading	Output
编号	信号源	单位	Start 开始	End 结束	(actual) 实际读数	value 产值
1	HCL	mg/N/m3	0	120	60.21 ppm	60.21 PP
2	HF	ma/Nn3	0	5	4,32 ppm	4,32 ppm
3	СО	ma/Nm3	0	1000	128.20 ppm	128.20 00
4	NO	ma/Nm3	0	500	122,00 PPh	122,00 ppm
5	NO ₂	ma/Nm3	0	200	98.80 ppin	98.81 PD
6	NO _X	mal Nm2	0	500	4/2,22 mg/m	4/2,2/my/
7	SO ₂	ma/Nm3	(2)	300	83,21 PPm	83.21 PPIn
8	CO ₂	10/0/0	0	25	20.000/0	20.00 0/0
9	H ₂ O	Vol do	0	40	32.0/0/0	32,01 0/8
10	O ₂	Vol 0/0	0	21	20,950/0	20,950/0
11	TOC	ma/Nm3	0	300	122,01 PPM	122,01 pm
12	NH ₃	ma/Nin3	0	100	53,30 PPM	53,30 PP
13	CH4	mg/Nm3	0	100	112.02 PPM	112,02 pp
14		37.7.01			113	1
15						

Remarks 备注		
Date	118	Name 签名
Date 日期: 25/7/2018 Engineer 工程师: Lullie Luw	Plant personnel 用户代表:	w.

		ns and their n Span Gas	Carbon Dioxide (CO2)	Oxygen (O2)	Methane (CH4)	Carbon Monoxide (CO)	Nitric Oxide (NO)	Sulphur Dioxide (SO2)	Nitrogen Dioxide (NO2)	Hydrogen Chloride (HCl)	Ammonia (NH3)	Hydrogen Floride (HF)	Propane (C3H8
Cal. Date and Line#			20	2.1	839	128.2	122	83.2	98.8	60.2	53.3	4.31	1117
07/May/2019	L1	Before				129.81	135.82	81.84	97.86	X			
07/Way/2013		After				127.93	123.07	83.37	99.1				
07/May/2019	L2	Before				126.03	118.64	82.58	97.71				
07/1VIAY/2019	LZ	After				129.02	122.17	83.17	98.57				
09/May/2019	L1	Before									52.15		
09/Way/2019	LT	After									53.17		
09/May/2019	L2	Before									51.76		
09/Way/2019	LZ	After									54.01		
05/Jun/2019	L1	Before	T-V	2.5									
05/1011/2019	LT	After		2.1									
05/Jun/2019	L2	Before		2.4									
05/1011/2019	LZ	After		2.1									
	L1	Before				,							
		After											
	L2	Before											
	LZ	After		•									
	L1	Before											
		After											
	L2	Before											
	LZ	After											
	L1	Before											
		After											
	L2	Before											
	LZ	After											
	L1	Before											
	LI	After											
	L2	Before											
	LZ	After											
	L1	Before											
		After											
	L2	Before											
	LZ	After											
	14	Before			7				A I V - T TE				
	L1	After											
		Before					1						
	L2	After											

Annex C2

Calibration Certification for the CAPCS

QM Zertifikat / QM certificate

Dusthunter SP30



Identifikation / identification

Artikel Nr. / Part No.:

1089203

DHSP30-T2V2FPNNNNNXXS

败

Ident Nr. / Ident no :

00116

Serien Nr. / Serial no.:

18168223

Firmware Version / Firmware version:

01.02.06 (Feb 27 2018 11:37:54)

Hardware Revision / Hardware version:

1.2

1

Geräteausführung / Device version:

BUS-Adresse / Bus address:

Bootloader Version / Bootloader version: 01.00.02

Parameter / Parameter

Sensorantwortzeit Sensor response time 60.0 sec.

Gebläse / Blower:

SN: 00014 / 08518553

Spantest 70 Laser /

Span 70 Laser

Relais 3:

installiert

installed

Referenzgerät Streulicht DHSP100 Serien-Nr.: Reference measuring device DHSP100 Serial no.:

Messgrößen u. Koeffizienten / Measuring variables and coefficients

Streulichtfaktoren / Scattered light coefficients:

CC0 (abs.):

-0.3800

CC1 (lin.):

Gain 0:

0.6850

CC2 (square):

0.0000

Verstärkungsfaktor, Offset / Gain factor, Offset:

10.0000

Offset 0: 0.00045

Faktoren Analogausgang / Analog Output factors:

CC0 (abs.): CC1 (lin.):

2.00 170.85

CC2 (square):

0.00

Koeffizientensätze Messbereich 0 / Coefficient Sets meas. range 0:

Koeff. Satz 1 / Coeff. set 1:

0.0000

CC 0 (abs.): CC 1 (lin.):

1.0000 0.0000

CC 2 (square):

CC 0 (abs.):

CC 1 (lin.):

CC 2 (square):

1.0000

0.0000

70.00 %

Wartung / Maintenance

0.0000

Messbereich, Grenzwert / Meas. range, limit:

Koeff, Satz 2 / Coeff, set 2:

Protokoll / protocol:

Modbus Schnittstelle / Modbus interface:

RTU

Meas. range switch: Messbereich Wert1 /

0.0 mg

0 (Software)

Adresse / address:

1

Meas. range low value:

Messbereichsschalter /

Baudrate / baudrate: Datenbits Parität Stopbits 19200

Messbereich Wert2 /

75.0 mg

/ Databits parity stopbits:

8 EVEN 1

Meas. range high value:

Endian Codierung / endian code:

NONE

Grenzwert / Limit value:

50.0 mg

Gebläse Druck/Blower Pressure:

10.0 mbar

Das Gerät mit der o.g. Serien-Nr. wurde überprüft und kalibriert nach den Qualitätsstandards der SICK-Gruppe basierend auf einem nach ISO9001 zertifizierten Qualitätssicherungssystem.

This device with the serial no. noted above has been tested and calibrated according to the quality standards of the SICK-Group, which are based on a ISO9001 certified Quality Assurance System.

Ottendorf-Okrilla, 16.04.2018

Unterschrift:

Signature:



Annex D

Implementation Schedule of Mitigation Measures

Annex D Summary of Mitigation Measures Implementation Schedule for Operation Phase

EIA Ref.	EM&A	Environmental Protection Measures	Location/ Timing	Status
	Log Ref.			
	·	al Mitigation Measures in the EIA and EM&A Manual		
	ir Quality		T	T 1
3.78	2.7 & 2.13 - 2.19	Air Pollution Control (Construction Dust) Regulation & Good Site Practices	OWTF Stacks/ During	V
	- 2.19	•Commissioning tests shall be conducted to confirm the centralized air pollution control unit,	Commissioning Stage	
		the cogen units, the standby flaring unit and ASP against the design emission levels as stated in Tables 2.2 - 2.5.		
		•Odour monitoring shall be conducted at the stack exhaust of the centralized air pollution		
2.70	2.7.2.12	control unit weekly in the first month of the commissioning stage.		
3.78	2.7-2.12	Air Pollution Control and Stack Monitoring	During Operation	V
		•Stack monitoring shall be installed for the centralized air pollution control unit, cogen units		
		and ASP of OWTF to ensure that the air emissions from OWTF would meet the design emission		
		limits as well as EPD criteria.		
3.78	2.20- 2.28	•Odour Patrol at site boundary of OWTF	OWTF Site Boundary/During	N/A
			Operation (The need to continue	
			the odour patrol after the end of	
			the 2-year monitoring period	
			would depend on the monitoring	
			results and should be agreed	
			with EPD)	
В. Н	lazard to Life	<u></u>	with El D)	<u> </u>
4.103	3.4	Operation Phase	Work Site / During Operation	V
		•3m high fence should be constructed along the boundary facing the SHWWTW	Period	
		•Emergency evacuation procedures should be formulated and the Contractor should ensure		
		on site staff should be familiar with these procedures. Diagram showing the escape routes to a		
		safe place should be posted in the site notice boards and at the entrance/exit of site. A copy of		
		the latest version emergency procedures should be dispatched to Tung Chung Fire Station for reference once available.		
		•The emergency procedures should specify means of providing a rapid and direct warning		
		(e.g. Siren and Flashing Light) to personnel on site in the event of chlorine gas release in the SHWWTW.		

EIA Ref.	EM&A	Environmental Protection Measures	Location/ Timing	Status
	Log Ref.			
		•The Contractor should establish a communication channel with the SHWWTW operation personnel and FSD. In case of any hazardous incidents in the treatment works, operation personnel of SHWWTW should advise the Contractor to inform personnel on site to proceed		
		with emergency procedure. The Contractor should appoint a Liaison Officer to communicate with FSD Incident Commander on site in case of emergency.		
		•Periodic drills should be coordinated and conducted to ensure all on site personnel are		
		familiar with the emergency procedures. Upon completion of the drills, a review on every		
		step taken should be conducted to identify area of improvement. Prior notice of periodic drills		
		should be given to Station Commander of Tung Chung Fire Station. Joint operational exercise		
		with FSD and SHWWTW is recommended.		
	later Quality	I W C O W . T P	T	
5.44	4.5	Wastewater from Organic Waste Treatment Process	Work Site / During Design &	V
		The Project site will be equipped with an adequately sized wastewater treatment plant. A	Operation Period	
		high rate type of active sludge system specifically designed for the removal of nitrogen components from the wastewater in combination with conversion of residual BOD and COD		
		would be deployed. The wastewater treatment plant would also be incorporated with		
		SHARON or annamox technology or equivalent to achieve high total overall nitrogen		
		removal. Wastewater generated from the OWTF (including wastewater from dewatering		
		process, leachate from waste reception area, condensate from biogas handling, wastewater		
		from scrubber of air treatment system and any surplus water from truck washing facility)		
		will be diverted to the wastewater treatment plant. Treated effluent will then be stored		
		temporarily in order to be used as process water within the plants. The storage volume		
		would be around 20 m3. Overflow from the tank will be discharged to foul sewers. The		
		polluting parameters in effluent shall be in compliance with the requirements specified in		
		the TM- DSS. The design, installation and operation of the wastewater treatment plant shall be licensed under the Waste Disposal Ordinance and subject to the effluent monitoring as		
		required under the WPCO which is under the ambit of regional office (RO) of EPD. To		
		ensure that wastewater can be adequately treated and effluent from treatment plant can		
		meet the standards listed in TM- DSS, the following mitigation measure should be		
		conducted.		
		Cleaning and maintenance of treatment facilities should be conducted on a regular		
		basis to ensure that removal rate of each treatment facility would not be reduced.		
		Cleaning and maintenance of pipelines should be carried out on a regular basis to		
		prevent block of pipeline and leaching of wastewater, and therefore prevent		
		overflowed or leached wastewater discharging into nearby drainages and water		
		streams.		
		Regular site inspection should be conducted to ensure that no wastewater can be directly discharged into property victor through		
		directly discharged into nearby water streams.		

EIA Ref.	EM&A	Environmental Protection Measures	Location/ Timing	Status
	Log Ref.			
5.55	4.5	In the scrubber, spraying water should be re-circulated to minimize the need for external water.	Work Site / During Design &	$\sqrt{}$
		The spraying water would be collected at the bottom of the scrubber. Excess water would be discharged to the wastewater treatment plant as described in Section 5.54.	Operation Period	
5.56	4.5	The waste reception, treatment facilities and compost storages of OWTF should be located in	Work Site / During Design &	√ √
		enclosed buildings to prevent generation of contaminated rain runoff. All surface runoff such	Operation Period	
		as washed water generated in the treatment processes areas should be properly collected and	_	
		diverted to the on-site wastewater treatment plant as described in Section 5.54.		
5.57	4.5	All drainage system for collection and transferring wastewater generated in the OWTF to the	Work Site / During Design &	$\sqrt{}$
		on-site wastewater treatment plant as described in Section 5.54 should be capable of preventing clogging and easy maintenance and cleaning.	Operation Period	
D. V	Vaste Managem		1	
6.50	5.12	Good Site Practices	During Operation Period	V
		Good operational practices should be adopted to Minimize waste management impacts:		
		•Obtain the necessary waste disposal permits from the appropriate authorities, in accordance		
		with the Waste Disposal Ordinance (Cap. 354), Waste Disposal (Chemical Waste) (General)		
		Regulation and the Land (Miscellaneous Provision) Ordinance (Cap. 28);		
		•Nomination of an approved person to be responsible for good site practice, arrangements for		
		collection and effective disposal to an appropriate facility of all wastes generated at the site;		
		•Use of a waste haulier licensed to collect specific category of waste;		
		•A trip-ticket system should be included as one of the contractual requirements and		
		implemented by the Environmental Team to monitor the disposal of solid wastes at public		
		filling facilities and landfills, and to control fly tipping. Reference should be made to ETWB		
		TCW No. 31/2004.		
		•Training of site personnel in proper waste management and chemical waste handling		
		procedures;		
		•Separation of chemical wastes for special handling and appropriate treatment at a licensed		
		facility;		
		•Routine cleaning and maintenance programme for drainage systems, sumps and oil		
		interceptors;		
		•Provision of sufficient waste disposal points and regular collection for disposal;		
		•Adoption of appropriate measures to minimize windblown litter and dust during		
		transportation of waste, such as covering trucks or transporting wastes in enclosed containers; and		
		•Implementation of a recording system for the amount of wastes generated, recycled and		

EIA Ref.	EM&A Log Ref.	Environmental Protection Measures	Location/ Timing	Status
		disposed of (including the disposal sites).		
6.51 5.13		Waste Reduction Measures Good management and control can prevent the generation of significant amounts of waste. It is recommended that the following good operational practices should be adopted to ensure waste reduction:	During Operation Period	√
		•Segregation and storage of different types of waste in different containers, skips or stockpiles		
		to enhance reuse or recycling of materials and their proper disposal;		
		•Encourage collection of aluminum cans, plastic bottles and packaging material (e.g. carton		
		boxes) and office paper by individual collectors. Separate labelled bins should be provided to help segregate this waste from other general refuse generated by the work force; and •Any unused chemicals or those with remaining functional capacity should be reused as far as		
		practicable.		
6.52	5.14	Wastes Generated from Pre-Treatment Process	Pre-Treatment Process/ During	 √
		Wastes generated from pre-treatment process should be recycled as far as possible. Wastes generated from pre- treatment process should also be separated from any chemical waste and stored in covered skips. The recyclables should be collected by licensed collectors, while the rest of the waste should be removed from the site on a daily basis to minimize odour, pest and litter impacts. Open burning must be strictly prohibited.	Operation Period	
6.53-6.56	5.15-5.18	<u>Chemical Wastes</u>	Whole Site / During Operation	√
		•Chemical waste generated from machinery maintenance and servicing should be managed in accordance with Code of Practice on the Packaging, Labelling and storage of Chemical Wastes under the provisions of Waste Disposal (Chemical Waste) (General) Regulation. The chemical waste should be collected by drum-type containers and removed by licensed chemical waste contractors.	Period	
		•Plant / equipment maintenance schedules should be planned in order to minimize the		
		generation of chemical waste.		
		•Non-recyclable chemical wastes and lubricants should be disposed of at appropriate facilities, such as CWTC. Copies or counterfoils from collection receipts issued by the licensed waste collector should be kept for recording purpose.		
		•Recyclable chemical waste will be transported off-site for treatment by a licensed collector. The Contractor will need to register with EPD as a chemical waste producer. Where possible, chemical wastes (e.g. waste lubricants) would be recycled at appropriate facilities, such as		
		Dunwell's oil re-refinery.		
6.57-6.58	5.19-5.20	General Refuse	Whole Site / During Operation	√

EIA Ref.	EM&A Log Ref.	Environmental Protection Measures	Location/ Timing	Status
		•Waste generated in offices should be reduced through segregation and collection of	Period	
		recyclables. To promote the recycling of wastes such as used paper, aluminum cans and plastic bottles, it is recommended that recycling bins should be clearly labelled and placed at locations with easy access. For the collection of recyclable materials, they should be collected by licensed collectors.		
		•General refuse, other than segregated recyclable wastes, should be separated from any		
		chemical waste and stored in covered skips. The general refuse should be removed from the site on a daily basis to minimize odour, pest and litter impacts. Also, open burning of refuse must be strictly prohibited.		
Е. Р		Contamination Preventive Measures		
6.65	5.21 (i)	 Fuel Oil Containers Fuel oil should be stored in suitable containers. All fuel oil containers should be securely closed. Appropriate labels showing the name of fuel oil should be posted on the containers. Drip trays should be provided for all containers. 	Fuel Oil Storage Containers /During Operation Period	√
6.65	5.21 (ii)	 Storage Area Distance between the fuel oil refuelling points and the fuel oil containers should be minimized. The storage area should be used for fuel oil storage only. No surface water drains or foul sewers should be connected to the storage area. The storage area should be enclosed by three sides by a wall and have an impermeable floor or surface. 	Fuel Oil Storage Area / During Operation Period	√
6.65	5.21 (iii)	Fuel Oil Spillage Response An Oil Spill Response Plan should be prepared by the operator to document the appropriate response procedures for oil spillage incident in detail. General procedures to be taken in case of fuel oil spillage are presented below. • Training Training on oil spill response actions should be given to relevant staff. The training should cover the followings: - Tools & resources to combat oil spillage and fire, e.g. locations of oil spill handling equipment and firefighting equipment; - General methods to deal with oil spillage and fire incidents; - Procedures for emergency drills in the event of oil spills and fire; and - Regular drills should be carried out. • Communication Establish communication channel with the Fire Services Department (FSD) and EPD to	Whole Site / During Operation Phase	√

EIA Ref.	EM&A	Environmental Protection Measures	Location/ Timing	Status
	Log Ref.			
		report any oil spillage incident so that necessary assistance from relevant department could be quickly sought. • Response Procedure Any fuel oil spillage within the Project Site should be immediately reported to the Site Manager with necessary details including location, source, possible cause and extent of the spillage Site Manager should immediately attend to the spillage and initiate any appropriate action to confine and clean up the spillage. The response procedures should include the following: - Identify and isolate the source of spillage as soon as possible. - Contain the oil spillage and avoid infiltration into soil / groundwater and discharge to storm water channels. - Remove the oil spillage. - Clean up the contaminated area. - If the oil spillage occurs during refuelling, the refuelling operation should immediately be stopped. - Recovered contaminated fuel oil and the associated material to remove the spilled oil should be considered as chemical waste. The handling and disposal procedures for chemical wastes are discussed in the following		
6.66	5.22 (i)	 Chemicals and Chemical Wastes Handling & Storage Chemicals and chemical wastes should only be stored in suitable containers in purpose-built areas. The storage of chemical wastes should comply with the requirements of the Code of Practice on the Packaging, Labelling and Storage of Chemical Wastes. The storage areas for chemicals and chemical wastes should have an impermeable floor or surface. The impermeable floor I surface should possess the following properties: Not liable to chemically react with the materials and their containers to be stored. Able to withstand normal loading and physical damage caused by container handling The integrity and condition of the impermeable floor or surface should be inspected at regular intervals to ensure that it is satisfactorily maintained For liquid chemicals and chemical wastes storage, the storage area should be bonded to contain at least 110% of the storage capacity of the largest containers or 20% of the total quantity of the chemicals/chemical wastes stored, whichever is the greater. 	Whole Site / During Operation Period	

EIA Ref.	EM&A Log Ref.	Environmental Protection Measures	Location/ Timing	Status
		 Storage container should be checked at regular intervals for their structural integrity and to ensure that the caps or fill points are tightly closed. Chemical handling should be conducted by trained workers under supervision. 		
6.66	5.22 (ii)	Chemicals and Chemical Wastes Spillage Response A Chemicals and / or Chemical Wastes Spillage Response Plan should be prepared by the operator to document in detail the appropriate response procedures for chemicals or chemical wastes spillage incidents. General procedures to be undertaken in case of chemicals I chemical wastes spillage incidents. General procedures to be undertaken in case of chemicals I chemical waste spillages are presented below • Training • Training on spill response actions should be given to relevant staff. The training should cover the followings: - Tools & resources to handle spillage, e.g. locations of spill handling equipment; - General methods to deal with spillage; and - Procedures for emergency drills in the event of spills. • Communication Establish communication channel with Fire Services Department (FSD) and EPD to report the spillage incident so that necessary assistance from relevant department could be quickly sought. • Response Procedures Any spillage within OWTF site should be reported to the Site Manager. Site Manager shall attend to the spillage and initiate any appropriate actions needed to confine and clean up the spillage. The response procedures should include the followings: - Identify and isolate the source of spillage as soon as possible; - Contain the spillage and avoid infiltration into soil / groundwater and discharge to storm water channels (in case the spillage occurs at locations out of the designated storage areas); - Remove the spillage; the removal method / procedures documented in the Material Safety Data Sheet (MSDS) of the chemicals spilled should be observed; - Clean up the contaminated area (in case the spillage occurs at locations out of the designated storage areas); and - The waste arising from the cleanup operation should be considered as chemical wastes.	Whole Site / During Operation Period	
6.67 - 6.69	5.23- 5.25	Incident Record • After any spillage, an incident report should be prepared by the Site Manager. The incident report should contain details of the incident including the cause of the	Whole Site / During Operation Period	√

EIA Ref.	EM&A	Environmental Protection Measures	Location/ Timing	Status
	Log Ref.			
		 incident, the material spilled and estimated spillage amount, and also the response actions undertaken. The incident record should be kept carefully and able to be retrieved when necessary. The incident report should provide sufficient details for the evaluation of any environmental impacts due to the spillage and assessment of the effectiveness of measures taken. In case any spillage or accidents results in significant land contamination, EPD should be informed immediately and the Project operator should be responsible for the cleanup of the affected area. The responses procedures described in Sections 6.65 - 6.66 of the EIA Report should be followed accordingly together with the land contamination assessment and remediation guidelines stipulated in the Guidance Manual for Use of Risk-based Remediation Goals for Contaminated Land Management and the Guidance Note for Contaminated Land Assessment and Remediation. 		
	andscape and V			
7.98 & Table 7.8	Table 6.2	 Operation Phase Aesthetic design of the facade, including its colour theme, pattern, texture, materials, finishing and associated structures to harmonize with the surrounding settings Grass / groundcover planting to soften the roof Heavy standard tree planting to screen proposed associated structures Grasscrete paving to soften the harshness of large paved surface areas wherever possible 	Within Project Area / During Design & Operation Stages	

Remark:

- √ Compliance of Mitigation Measures
- Compliance of Mitigation but need improvement
- x Non-compliance of Mitigation Measures
- ▲ Non-compliance of Mitigation Measures but rectified by OSCAR Bioenergy JV
- Δ Deficiency of Mitigation Measures but rectified by OSCAR Bioenergy JV
- N/A Not Applicable in Reporting Period

Annex E

Waste Flow Table

No. EP/SP/61/10 of Organic Resources Recovery Centre (Phase 1) Monthly Summary Waste Flow Table

		Was	te Generated from Pr	etreatment Process					Genera	l Refuse			
Month	Chemical Waste	Disposed of at Landfill (see Note 1)	Metals (see Note 2)	Paper/ cardboard packaging (see Note 2)	Plastics (see Note 3)	Dispose Landfill (se	ee Note 1	Metals (see	e Note 2)	Paper/ ca packaging 2)		Plasi (see No	
	Litre	tonne	tonne	tonne	tonne	No. of collection	tonne	No. of collection	tonne	No. of collection	tonne	No. of collection	tonne
March 2019	1,200	477.08	0	0	0	26	1.50	0	0	0	0	0	0
April 2019	0	455.60	0	0	0	22	1.27	0	0	0	0	0	0
May 2019	1,000	528.22	0	0	0	25	2.88	0	0	0	0	1	0.39
June 2019	0	459.23	0	0	0	24	2.76	0	0	0	0	0	0
July 2019	0	521.79	0	0	0	26	3.00	0	0	0	0	0	0
August 2019	40	441.05	0	0	0	27	3.11	0	0	0	0	0	0
September 2019	1,800	576.28	0	0	0	24	2.76	0	0	0	0	0	0
October 2019	0	441.22	0	0	0	25	2.88	0	0	0	0	0	0
November 2019	1,600	451.57	0	0	0	26	3.00	0	0	0	0	0	0
December 2019	1,009	488.13	0	0	0	24	2.76	0	0	0	0	0	0
January 2020	0	388.20	0	0	0	23	2.65	0	0	0	0	0	0
February 2020	4,525	372.97	0	0	0	24	2.76	0	0	0	0	0	0
March 2020	1,200	351.71	0	0	0	27	3.11	0	0	0	0	0	0
April 2020	0	363.92	0	0	0	21	2.42	0	0	0	0	0	0
May 2020	800	294.36	0	0	0	25	2.88	0	0	0	0	0	0
June 2020	0	347.23	0	0	0	25	2.88	0	0	0	0	0	0
July 2020	200	852.07	0	0	0	26	3.00	0	0	0	0	0	0
August 2020	0	700.25	0	1.20	0	25	2.88	0	0	0	0	0	0
September 2020	400	579.64	0	5.31	0	26	3.00	0	0	0	0	0	0
October 2020	0	840.75	0	5.83	0	24	2.76	0	0	0	0	0	0
November 2020	0	688.20	0	0.80	0	25	2.88	0	0	0	0	0	0
December 2020	766	685.47	0	0	0	25	2.88	0	0	0	0	0	0
January 2021	1,800	634.00	0	0	0	25	2.88	0	0	0	0	0	0
February 2021	6,120	377.72	0	0	0	21	2.42	0	0	0	0	0	0
March 2021	6,000	325.21	0	0	0	27	3.11	0	0	0	0	0	0

		Waste Generated from Pretreatment Process				General Refuse											
Month	Chemical Waste	Disposed of at Landfill (see Note 1)	Metals (see Note 2)	Paper/ cardboard packaging (see Note 2)	Plastics (see Note 3)	Disposed of at Landfill (see Note 1 & 4)		Landfill (see Note 1		Landfill (see Note 1		Metals (see	e Note 2)	Paper/ ca packaging 2)	(see Note	Plast (see No	
	Litre	tonne	tonne	tonne	tonne	No. of collection	tonne	No. of collection	tonne	No. of collection	tonne	No. of collection	tonne				
April 2021	9,700	651.29	0	0	0	22	2.53	0	0	0	0	0	0				
May 2021	4,000	671.03	0	0	0	24	2.76	0	0	0	0	0	0				
Total	42,160.00	13,964,20	0	13.14	0	664	73.73	0	0	0	0	1	0.39				

Notes:

- 1. General refuse was disposed of at NENT by subcontractors.
- 2. Metal and paper/cardboard packaging were collected by recycler for recycling.
- 3. Plastics refer to plastic bottles/containers, plastic sheets/foam from packaging material collected by recycler for recycling.
- 4. It was assumed that four 240-litre bins filled with 80% of general refuse were collected at each collection. The general refuse density was assumed to be around 0.15 kg/L.

Annex F

Environmental Complaint, Environmental Summons and Persecution Log

Annex F Cumulative Complaint and Summons/Prosecutions Log

Reporting Month	Number of Complaints in Reporting Month	Number of Summons/Prosecutions in Reporting Month
May 2015	0	0
June 2015	0	0
July 2015	0	0
August 2015	0	0
September 2015	0	0
October 2015	0	0
November 2015	0	0
December 2015	0	0
January 2016	0	0
February 2016	0	0
March 2016	0	0
April 2016	0	0
May 2016	0	0
June 2016	0	0
July 2016	0	0
August 2016	0	0
September 2016	0	0
October 2016	0	0

Reporting Month	Number of Complaints in Reporting Month	Number of Summons/Prosecutions in Reporting Month
November 2016	0	0
December 2016	0	0
January 2017	0	0
February 2017	0	0
March 2017	0	0
April 2017	0	0
May 2017	0	0
June 2017	0	0
July 2017	0	0
August 2017	0	0
September 2017	0	0
October 2017	0	0
November 2017	0	0
December 2017	0	0
January 2018	0	0
February 2018	0	0
March 2018	0	0
April 2018	0	0
May 2018	0	0
June 2018	0	0

Reporting Month	Number of Complaints in Reporting Month	Number of Summons/Prosecutions in Reporting Month
July 2018	0	0
August 2018	0	0
September 2018	1	0
October 2018	0	0
November 2018	0	0
December 2018	0	0
January 2019	0	0
February 2019	0	0
March 2019	0	0
April 2019	0	0
May 2019	0	0
June 2019	0	0
July 2019	0	0
August 2019	0	0
September 2019	0	0
October 2019	0	0
November 2019	0	0
December 2019	0	0
January 2020	0	0
February 2020	0	0

Reporting Month	Number of Complaints in Reporting Month	Number of Summons/Prosecutions in Reporting Month
March 2020	0	0
April 2020	0	0
May 2020	0	0
June 2020	0	0
July 2020	0	0
August 2020	0	0
September 2020	0	0
October 2020	0	0
November 2020	0	0
December 2020	0	0
January 2021	0	0
February 2021	0	0
March 2021	0	0
April 2021	0	0
May 2021	0	0
Overall Total	1	0

Annex G

Investigation Report

Investigation Report of CEMS Exceedances

Date	1 - 31 May 2021
Time	Continuous monitoring throughout May 2021
Monitoring Location	Continuous Environmental Monitoring System (CEMS)
Parameter	Various emission parameters of the Cogeneration Unit (CHP)
	and Ammonia Stripping Plan (ASP)
Exceedance Description	1. Continuous monitoring was carried out at the CAPCS, CHP and ASP throughout the reporting period using the CEMS. According to the EM&A Manual, exceedance is
	considered if the emission concentration of the concerned pollutants is higher than the emission limits stated in Tables 2.2, 2.3 and 2.5 of the EM&A Manual (Version F) for CAPCS, CHP and ASP respectively. The
	concentration of the concerned air pollutants were monitored on-line by the CEMS. Exceedances of various emission parameters were recorded on the CEMS including:
	 NO_x, SO₂ and VOC in the CHPs
	 CO, NO_x, VOC and NH₃ in the ASP.
	2. According to the Contractor, exceedance is observed to
	occur mainly at CHPs operated at loading with 40-60% of
	the optimal loading (1400KW)
	3. The Contractor explained that the NO _x exceedances
	recorded in CHP 1 were due to the low biogas loading
	which results in the poor performance efficiency in CHP.
	4. The Contractor explained that the VOC and NO _x
	exceedances recorded in the CHP 3 were due to the
	unstable performance of the CHP. Although the
	Contractor was advised to halt the use of CHP 3 in this
	reporting period due to its unstable performance since
	the last reporting period, it was used when CHP 2 was
	under urgent maintenance for about 10 days as sufficient
	biogas consumption requires the operation of 2 CHPs.
	5. The Contractor explained that the CO, NO _x , VOC and
	NH ₃ exceedances in ASP were caused by unstable
	column temperature in biogas combustion, which have
	led to incomplete combustion of biogas and NH ₃ and
	hence exceedances in ASP.
	6. The SO ₂ exceedances recorded in CHPs were due to
	tripping of the desulphurisation system, which were
	stopped temporary for urgent maintenance. The desulphurisation system resumed to normal operation on
	the day after urgent maintenance.
Action Taken / Action to be	The quantity of SSOW has increased slightly with the
Taken	help of the EPD in this reporting month. The
	Contractor will continue to actively liaise with EPD in
	their monthly meeting with an aim to increase the
	The morning mooning with the increase the

	quantity of SSOW that can be treated daily, such that sufficient biogas can be generated for the CHP to be able to operate at optimal efficiency. • The Contractor has engaged with the CHP supplier to carry out an on-site inspection for the CHP by the supplier representative on 26 May 2021. The Contractor will continue to avoid the use of the CHP3 in the coming months when possible. • The Contractor has established a regular communication channel with the overseas ASP supplier, to overcome the fact that the supplier cannot travel to Hong Kong due to travel restriction. • The Contractor arranged for remote fine-tuning of the ASP with the overseas ASP supplier during this reporting period. • Daily meetings have been held to review ASP operational and emission data. • The Contractor will continue to arrange for remote fine-tuning of the ASP with the overseas contractor in the upcoming reporting period. The Contractor will continue to carry out maintenance measures as per the supplier's manual. • The Contractor in consultation with the overseas ASP supplier will investigate the reasons for the occasional equipment tripping that has led to unstable column temperature of the thermal oxidizer. The Contractor may carry out replacement of some ASP equipment and/or increase maintenance frequency, subject to their investigations.
Remedial Works and	The Contractor is recommended to closely monitor the
Follow-up Actions	processes, including the modification works and follow-up emission monitoring of the CHP and ASP to avoid exceedance.
	MT has advised that the issue of emission exceedances should
	be prioritised in up-coming meetings. MT will carry out
	follow-up audit regarding the progress next month.

Prepared by:	Angela Yung, MT Representative
Date	11 June 2021